Fall 1998

Evaluation of rotating fluidized bed as a dry coater

William Christopher Dunphy
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ABSTRACT

Coating of particles is normally carried out with the use of environmentally unfriendly solvents. Development of dry coating methods is therefore quite important.

A Rotating Fluidized Bed was constructed, instrumented and verified as to operation. Twelve coating experiments were carried out with PMMA 200µm mean diameter as host and alumina 0.25 µm primary particle size as guest with the RFB being operated in the fully fluidized range.

In all analyzed samples, coating was observed. Analysis was carried out on the qualitative basis by SEM and EDX.
EVALUATION OF ROTATING FLUIDIZED BED AS A DRY COATER

by

William Christopher Dunphy

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Submitted to the Faculty of
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in Partial Fulfillment of the Requirements for the Degree of
Master of Science in Mechanical Engineering

Department of Mechanical Engineering

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EVALUATION OF ROTATING FLUIDIZED BED AS A DRY COATER

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Watano, Pfeffer, Dave and Dunphy, “Dry Particle Coating by a Newly Developed Rotating Fluidized Bed Coater” Proceedings from AIChE Convention, Florida, November 1998
This thesis is dedicated to my family; to my Mother, without her help this thesis would have been impossible, to my Father, I wish he were here to read this thesis, and to my siblings, John, Gene, Jim and Dawn, their undying support made this journey easier. Also to my friends who kept me from going insane, especially Tom, Bill and Dr. John Gilchrist, without their infinite patience none of this would exist. Octavius Ad Infinum
ACKNOWLEDGMENT

I would like to express my deepest appreciation to Dr. Rajesh Dave and Dr. Robert Pfeffer, who not only served as my research supervisors, providing valuable and countless resources, insight and intuition, but also for constantly providing support, encouragement and reassurance. Special thanks is given to Dr. Pushpendra Singh for participating in my committee and especially for being a friend. I also wish to thank Dr. Sudhi Mukherjee for going out of his way to help.
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CHAPTER 1

INTRODUCTION

1.1 Objective
The objective of this thesis is to evaluate the Rotating Fluidized Bed (RFB) as a dry coating (RFBC) machine. It is believed that the magnification of the impact forces by RFB technology will create enough shear and normal forces to coat a guest onto a host. The shear force, to deagglomerate and smear the guest onto the host, and the normal force to impregnate the guest into the hosts surface.

There are two main components to this thesis. First a laboratory scale rotating fluidized bed has been designed, constructed and instrumented for data acquisition. In the second part of this thesis, the performance of the RFB is verified and evaluated as a dry coating machine using 200µm PMMA as host and 5% 0.25µm primary alumina as guest.

1.2 Motivation
Most current methods of coating are carried out in a wet form. Colloidal systems and spray type systems as well as others usually employ a volatile and toxic solvent that must be evaporated off into the atmosphere and/or stored as toxic waste. For example, a Wurster type coater [8] is a standard type fluidized bed with a center tube where the coating guest is in a suspension that is sprayed into the system,
leaving the solvent to be evaporated off into the atmosphere or to be captured by expensive equipment.

Dry coating uses no solvent and produces no residue that must be stored. This should be viewed as an important development in light of current environmental regulations both self imposed and government imposed.

1.3 Background Information

Fluidization is the operation by which fine solids are transformed into a fluid like state through contact with a gas or liquid [4]. This was first proven by Fraser and Yancey in 1928 [4]. A fluidized bed has the following positive characteristics;

- Superior mixing
- High rate of heat transfer
- Temperature uniformity
- Accelerated reaction due to available surface area
- Lower pressure drop than fixed bed

The RFB has all the desirable characteristics of a standard fluidized bed plus the ability to replace the gravity term in the standard bed equation by a centrifugal term (see Appendix C) which can be adjusted by increasing or decreasing the rate of rotation of the distributor.

Consider a standard fluidized bed (see Fig 1.3). It consists of a tube with a distributor (porous ceramic, sintered metal, wire cloth etc...) fixed near the bottom. Fluidization gas is introduced at the bottom at superficial velocity \( U_0 \) and passes through the distributor and then through the particle bed which rests on the
distributor. At zero velocity and until minimum fluidization velocity, Umf, the bed is said to be packed. At this point, Umf, the bed enters the fully fluidized regime. This regime is marked by a characteristic plateau where the whole bed is fluidized. At the time of fluidization, bubbling starts, but is negligible until some Umb when bubbling becomes vigorous (see chapter 3). After the bubbling reaches a certain point, entrainment (elutration) begins and material is ejected.

In a RFB the centrifugal force increases with depth in the bed. The bed remains packed until a minimum velocity Umf, when the inner surface of the bed fluidizes. When the superficial velocity reaches a critical velocity Umfc, the whole bed is fluidized. It is also at this point that bubbling begins, but it is negligible up to Umb (see Fig 1.2). When the velocity reaches Ume, elutration begins.
Fig. 1.3 Standard fluidized bed with free body diagram and force balance
The force balance can be written as:

\[ mg = F_b + F_d \]
\[ mg = \rho_g g V + F_d \]
\[ mg - \rho_g g V = F_d \]
\[ (m - \rho_g V)g = F_d \]

As can be seen by the force balance, the only thing that can be done to increase the flow rate of fluidization gas, and therefore the aerodynamic drag, is to increase the effective acceleration of gravity.

This can be achieved by rolling the distributor into a cylinder and rotating it as in the RFB (see Fig 1.4). The force balance for the RFB can be written as:

\[ m \omega^2 r = F_b + F_d \]
\[ m \omega^2 r = \rho_g \omega^2 r V + F_d \]
\[ m \omega^2 r - \rho_g \omega^2 r V = F_d \]
\[ (m - \rho_g V) \omega^2 r = F_d \]

By increasing the angular velocity of the bed the aerodynamic drag force must be increased to achieve fluidization, this in turn magnifies the impact forces. This feat can be achieved by placing endcaps on the cylindrical distributor, one with an exhaust outlet, and placing the assembly in a pressurized plenum. Thus the flow is directed through the bed.
Fig 1.3 Rotating fluidized bed side view (top) and front view (bottom) with free body diagram and force balance

\[ mw^2 r = F_b + F_d \]
As can be seen in the force balance, the higher the rotation rate, the more gas can be passed through the bed.

This increase in gas flow coupled with the increased effective weight will induce vigorous mixing accompanied by increased impact forces, most importantly shear. It is this shear which will do most of the coating of the host onto the guest.
2.1 Statement of Problem

In order that the machine be a rotating fluidized bed the following criteria must be met:

- The distributor must be cylindrical
- The distributor must be rotated during operation
- The distributor must rotate inside a pressurized plenum during operation
- The inside of the distributor must be exhausted to the outside of the plenum

2.2 Choice of Materials

As sample size is to be kept small, about 30 grams, a readily available thin wall steel cylinder of 2.25 inch inner diameter and 3 inch length was chosen to be used as a distributor. The plenum must be of appropriate size as to contain the distributor, a readily available 4 inch PVC schedule 40 pipe was selected. During prototyping it was decided that the bed should be visible from the outside during operation so readily available acrylic sheeting was selected for distributor end plates and plenum housing end plates as well as the hatch in the front plenum end plate. In order that the plenum be sealed around the rotating exhaust nozzle, a
special seal made of moly impregnated fiberglass was constructed by National Ready Seal. The shaft was made of readily available 1/2 inch drill rod. Teflon® bushings were procured for rear plenum plate penetration point and exhaust nozzle. It was later discovered that the seal and nozzle were of incompatible material so a stainless steel Ready Sleeve® was fitted to the exhaust nozzle. The PVC plenum chamber was gasketed to the acrylic end plates using red rubber plumbers gasket. The bearings were easily procured mounted in pillow blocks from a machinist’s supply. The motor was a Dayton DC model with RPM controller. All parts were mounted to a 2 X 12 inch yellow pine plank.

2.3 Engineering Analysis of Particle Forces

G forces imparted on particle at wall of distributor;

\[ F = ma = m r \omega^2 \]  
\[ a = r \omega^2 = \frac{57.15 \times 10^{-3} m \times (RPM \times \frac{\pi}{30})^2 \times \frac{1}{9.81 \frac{m}{s^2}}} {2} \]  

<table>
<thead>
<tr>
<th>RPM</th>
<th>a [g]</th>
</tr>
</thead>
<tbody>
<tr>
<td>300</td>
<td>3</td>
</tr>
<tr>
<td>600</td>
<td>11.5</td>
</tr>
<tr>
<td>900</td>
<td>26</td>
</tr>
<tr>
<td>1200</td>
<td>46</td>
</tr>
<tr>
<td>1500</td>
<td>72</td>
</tr>
</tbody>
</table>
2.4 Choosing Convenient Dimensions

In order that the RFB be built with a minimum of special tools, all components purchased were selected with respect to each other and with respect to available cutting tools. The motor had a 5/8 inch output shaft and the drive shaft selected for the RFB was 1/2 inch. A rubber coupler was commercially available to join the two. The drive shaft bearings were pillow block units and were available in the required 1/2 inch inner diameter size. A Teflon® bushing of 1/2 inch ID and 3/4 inch OD was selected to bush the drive shaft through the rear plenum plate, another bushing selected from the same series of 1 inch ID and 1 1/4 inch OD served as the exhaust nozzle. These selections were viewed as excellent as the rear bushing would not have to be lubricated so as to ward off contamination of the sample. The same view was taken with the bushing that was to serve as exhaust nozzle, but, a poor choice of seal material by National Ready Seal engineers required that a Ready Sleeve® made of stainless steel be installed over the nozzle. Another parameter was also satisfied by virtue of convenient dimensions on the OD of the bushings as they were of readily available drill sizes.

2.5 Manufacture of RFB

The only special tools used in the manufacture of the RFB prototype were a Craftsman® router table and router, and a small drill press. Fixtures were made with a flat board and wooden dowels to make the perfectly circular end caps for
the distributor, and to make the circular recesses in the end plates for the plenum.
The correct size center holes were drilled into the acrylic plastic and were passed by the router bit by hand.

In order that the distributor be slotted properly, a 1/4 inch four flute end mill was fitted to the router table. A fixture made of red oak was slotted and eased on the top edge and the pre drilled steel distributor cylinder was screwed down firmly and the whole fixture was passed over the end mill by hand.

The use of threaded rod was maximized so as to reduce the cost of manufacture. All components are held together and mounted using threaded rod.
CHAPTER 3

VERIFICATION OF RFB

3.1 Generation of Fluidization Curve

In order that the RFB built in this thesis actually performs as a rotating fluidized bed, and, to insure that the coating attempt be made in the fluidized region, fluidization curves must be generated for this machine.

The first step in generating the fluidization curves is to take differential manometer readings at incremental steps of air flow with the distributor empty. After this is performed at all desired rotation speeds, the distributor is loaded with a 30 gram sample of the 200µm PMMA host. The RFB is then run and manometer readings taken at the same air flow increments as previous. The data is then subtracted, the data points generated with the empty distributor are subtracted from the points taken with the sample in the distributor. These points are then graphed on the ordinate while the equivalent superficial velocity with respect to air flow are graphed on the abscissa (see Fig 1.1).

If one consults the fluidization graph, one can see the reasonably linear packed bed region clearly. Next is the partially fluidized regime. This is followed in most cases by a fully fluidized plateau. This is most evident in the 600 RPM graph and is absent in the 1500 RPM graph. During the fully fluidized plateau regime, the bubbling regime takes place. The bubbling is negligible in the beginning and gradually increases until elutriation (entrainment or ejection). This type of
behavior is typical of Geldart type A particles [9]. It should be noted that in a Rotating Fluidized Bed, heavy bubbling can lead to entrainment as when a bubble bursts the particles are flung up into the distributor and are disconnected from their effective acceleration leaving them too light to remain in the system.

![Fluidization Graph](image)

**Fig. 3.1 Experimental calibration data**

It can be seen that for 600 RPM full fluidization occurs at approximately 12 cm/s and ends at approximately 36 cm/s followed by the bubbling regime. For 900 RPM full fluidization starts at approximately 25 cm/s and ends at approximately 36 cm/s followed by its bubbling regime. For 1200 RPM full fluidization begins at approximately 35 cm/s and ends at approximately 40 cm/s followed by its bubbling regime. 1500 RPM exhibits no plateau, this RFB is incapable of safely handling the pressure difference and therefore the superficial velocity to fluidize this material at this RPM.
3.2 Comparison of Experimental Data to Theory

The accepted model of Rotating Fluidization is derived from the Ergun equation, the following derivation is taken from [1]. Pressure drop as a function of superficial gas velocity is based on the semiempirical equations of Chen [8] modified by Kao [1]. In the packed bed region, the pressure drop is given by;

\[
\frac{dP}{dr} = \phi_1 \left( \frac{U_o r_o}{r} \right) + \phi_2 \left( \frac{U_o \sigma r_o}{r} \right)^2 + \frac{\rho_f r \omega^2}{\varepsilon^2 r_o^3} + \frac{\rho_f U_o^2 r_o^2}{\varepsilon^2 r_o^3}
\]

Where;

\[
\phi_1 = \frac{150(1 - \varepsilon)^2 \mu}{\varepsilon^3 \left( \phi_d d_g \right)^2}; \phi_2 = \frac{1.75(1 - \varepsilon) \rho_f}{\varepsilon^3 \phi_d d_g}
\]

Which is based on the Ergun equation. The major contribution is from the drag force per unit volume, that is the first two terms. The remaining two terms add up to less that one percent and may be neglected. Now we are left with;

\[
\frac{dP}{dr} = \phi_1 \left( \frac{U_o r_o}{r} \right) + \phi_2 \left( \frac{U_o \sigma r_o}{r} \right)^2 
\]

Which is integrated thus;

\[
\int_{R_1}^{R_2} dP = \phi_1 U_o r_o \int_{r}^{R_2} \frac{dr}{r} + \phi_2 U_o^2 r_o^2 \int_{r}^{R_2} \frac{dr}{r^2}
\]

Which results in;

\[
\Delta P = \phi_1 U_o r_o \ln \left( \frac{r_o}{r_i} \right) + \phi_2 U_o^2 r_o^2 \left( \frac{1}{r_i} - \frac{1}{r_o} \right)
\]

For the fully fluidized plateau the original equation takes the form of;
\[
\frac{dP}{dr} = (\rho_g - \rho_f)(1 - \varepsilon) r \omega^2 + \rho_f g r \omega^2 + \frac{\rho_f U^2 r_e^2}{\varepsilon^3} + \frac{\rho_f U^2 r_e^2}{\varepsilon^2 r^2} \frac{d\varepsilon}{dr}
\]

And as in the packed bed region, the three right terms are negligible resulting in;

\[
\frac{dP}{dr} = (\rho_g - \rho_f)(1 - \varepsilon) r \omega^2
\]

Integrating;

\[
\int_{r_1}^{r_2} dP = (\rho_g - \rho_f)(1 - \varepsilon) \omega^2 \int_{r_1}^{r_2} r \, dr
\]

Which results in;

\[
\Delta P = (1 - \varepsilon)(\rho_g - \rho_f) \omega^2 (r_2^2 - r_1^2) / 2
\]

### 3.3 Graphical Comparison

The above equations are graphed along with the experimental data in order that a comparison be made. A void fraction of 4.2 was found to be a good approximation, verifying Wen and Yu’s correlation [11]. To make up the difference between actual and ideal situations a fully fluidized correction factor of 0.78 provided good agreement of the data with the theory. In the following graphs, series 1 is the experimental data, series 2 is the fully fluidized theory and series 3 is the packed bed theory. Because of the unwieldy nature of the partially fluidized theory equation it is omitted in these graphs (see appendix C).

The three rotometers used to regulate the mass flow of air into the system behaved in different ways. Meter one and two regulated up to 600 SCFH and were steady and easy to use. However, meter three that regulated from 600 SCFH
and above had wild fluctuations and may have contributed to the bubbling and elutration from that point on. If $Q = 600$ SCFH then $U_0 = 34.5622$ cm/s.

**Experimental VS. Theoretical Using Ergun Equation; 600 RPM**

![Graph showing comparison of theory to data 600 RPM](image)

**Fig 3.2 Comparison of theory to data 600 RPM**

Good agreement of packed bed equation accompanied by an underestimation of the fully fluidized plateau. Heavy bubbling is evident before the ejection region.
Experimental VS. Theoretical Using Ergun Equation; 900 RPM

Fig. 3.3 Comparison of theory to data 900 RPM

Excellent agreement in both packed bed and fully fluidized plateau.

Experimental VS. Theoretical Using Ergun Equation; 1200 RPM

Fig. 3.4 Comparison of theory to data 1200 RPM
Good agreement in packed bed region accompanied by an ambiguous fully fluidized region.

**Experimental VS. Theoretical Using Ergun Equation; 1500 RPM**

![Graph showing comparison of theory to data at 1500 RPM](image)

**Fig. 3.5 Comparison of theory to data 1500 RPM**

Good agreement during initial packed bed region accompanied by divergence, no fully fluidized plateau realized.
CHAPTER 4

COATING EXPERIMENTS

4.1 Choice of Rotation Speed

Out of four speeds tested in chapter 3, two were selected for coating attempts, 900 RPM and 1200 RPM. 600 RPM exhibits a long and flat plateau where operation of the RFB in the fluidized region would be easily accomplished, but, the fact that only 3g's are generated by the rotation dictates that a higher RPM is needed for coating to occur. 1500 RPM was discarded as there was no fluidization present.

4.2 Choice of Fluidization Velocity

Experiments were run at a multiple of minimum fluidization velocity. For 900 RPM the values ranged from 600 SCFH to 720 SCFH. For 1200 RPM the values ranged from 780 SCFH to 1000 SCFH. If one checks the fluidization graph from chapter 3, some of these values are within the bubbling and/or ejection region for PMMA alone. The reason for this is that the presence of alumina seems to change the system sufficiently to prevent ejection, and, after performing the experiment in the fluidization region it was decided to raise the flow rate to maximize the interparticle forces. Future researchers of this topic should note that perhaps calibration of the RFB with the binary system would be more appropriate. This increase is acceptable as after processing almost all of the sample remained in the bed. This decision was made after observing the angle of repose of the sample
after processing. It was felt that the first three runs could have had a larger increase in AOR had a higher gas flow rate been used. The latter experiments exhibited an increased AOR as compared to the first three. These AOR measurements were made by eye in the sample jar.

4.3 Experimental Grid

The 12 experiments were carried out as follows:

<table>
<thead>
<tr>
<th>Exp. #</th>
<th>Δp [mm H2O]</th>
<th>RPM</th>
<th>Run Time [min.]</th>
<th>Uo [cm/s]</th>
<th>Q [SCFH]</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>72</td>
<td>900</td>
<td>10</td>
<td>34.5622</td>
<td>600</td>
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<tr>
<td>2</td>
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<td>4</td>
<td>110</td>
<td>900</td>
<td>10</td>
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</tr>
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<td>128</td>
<td>900</td>
<td>20</td>
<td>37.4424</td>
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</tr>
<tr>
<td>6</td>
<td>128</td>
<td>900</td>
<td>30</td>
<td>37.4424</td>
<td>650</td>
</tr>
<tr>
<td>7</td>
<td>156</td>
<td>1200</td>
<td>10</td>
<td>44.9309</td>
<td>780</td>
</tr>
<tr>
<td>8</td>
<td>156</td>
<td>1200</td>
<td>20</td>
<td>44.9309</td>
<td>780</td>
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<td>248</td>
<td>1200</td>
<td>30</td>
<td>57.6037</td>
<td>1000</td>
</tr>
</tbody>
</table>
4.4 Results

Although only a qualitative analysis was possible results were considered good. The RFB was verified and coating of alumina on PMMA was achieved. Looking at the raw SEM images in Appendix B, coating or an ordered mixture has clearly taken place on all samples tested. Due to limited time for SEM analysis, only seven of the twelve raw runs were analyzed.

In order that the coating condition be verified, three samples were sonicated for one minute in tap water and then subjected to further SEM analysis followed by EDX elemental mapping for aluminum.

Comparing sample #12 before and after sonication (see fig 4.1), the image on the right appears to retain coating despite sonication of the raw sample on the left. This shows that this is not just an ordered mixture but actual dry coating has taken place.
Although still a qualitative test, an EDX elemental mapping was carried out on all three batches that were sonicated. In all three cases, coating was observed. Shown in Fig. 4.2 is sample #10 run for 10 min. (see chapter 4.3) and exhibits a reasonable amount of discreet coating. Sample #12 in Fig. 4.4 is run at the same settings (RPM and Q) for 30 min and shows a heavier coating. This suggests that coating increases with time (see Fig. 4.5). Sample #11 (Fig. 4.3) shows an unfamiliar heavy and flaky unsymmetric coating and is considered anomalous and is being disregarded in these results.
Fig 4.2 Sample #10 sonicated for 1 min. SEM/EDX for Al

Fig 4.3 Sample #11 sonicated for 1 min. SEM/EDX for Al
4.5 Conclusions and Recommendations

This thesis has established the RFB as a feasible method to carry out dry coating. Coating condition requires further analysis as does thickness of coating with respect to time. Scale up of this RFB technology needs to be investigated as well.
as a continuous process instead of a batch system. Most important of all would be to identify and describe the mechanism of coating in the RFB.
APPENDIX A

DETAIL DRAWINGS
Fig A.1 RFB assembly (hidden line)
DISTRIBUTOR CAN BE SLOTTED OR DRILLED WITH WIRE CLOTH CEMENTED INSIDE OR DISTRIBUTOR CAN BE WOUND OUT OF SINTERED WIRE CLOTH
Fig A.3 front distributor plate

ROTATING FLUIDIZED BED COATING MACHINE
NJIT PTC/PPRC
FRONT DISTRIBUTOR PLATE
INCH W.C. DUNPHY 8/98
Fig. 4.6 exhaust nozzle retainer
NOTE: COMMERCIALLY AVAILABLE SHAFT COLLAR

Fig A.7 shaft collar

NOTE: COMMERCIALLY AVAILABLE SHAFT COLLAR

ROTATING FLUIDIZED BED COATING MACHINE

NJIT PTC/PPRC SHAFT COLLAR

INCH W.C. DUNPHY 8/98
MATERIAL: RED RUBBER PLUMBER'S GASKET
Fig A.14 front plenum plate
APPENDIX B

S.E.M. IMAGES
Fig B.1 raw alumina SEM
Fig B.2 raw PMMA SEM
Fig B.3 sample #1 raw SEM
Fig B.4 sample #2 raw SEM
Fig B.5 sample #3 raw SEM
Fig B.6 sample #4 raw SEM
Fig B.7 sample #5 raw SEM
Fig B.8 sample #6 raw SEM
Fig B.9 sample #7 raw SEM
Fig B.10 sample #12 raw SEM
Fig B.11 sample #10 sonicated SEM
Fig B.12 sample #11 sonicated SEM
Fig B.13 sample #12 sonicated SEM
Fig B.14 sample #10 sonicated EDX Al

Fig B.15 sample #11 sonicated EDX Al
Fig B.16 sample #12 sonicated EDX Al
APPENDIX C

DERIVATION OF FLUIDIZATION EQUATIONS

Taken from [1]

In the fixed bed region the pressure drop is given by the Ergun equation,

\[ \frac{dP}{dr} = \phi_1 \left( \frac{U_o r_o}{r} \right) + \phi_2 \left( \frac{U_o r_o}{r} \right)^2 + \rho_f r \omega^2 + \frac{\rho_f U_o^2 r_o^2}{\varepsilon^2 r^3} \]

where;

\[ \phi_1 = \frac{150(1 - \varepsilon)^2 \mu}{\varepsilon^3 \left( \frac{1}{\phi_3 d_s} \right)^2} ; \phi_2 = \frac{1.75(1 - \varepsilon) \rho_f}{\varepsilon^3 \phi_3 d_s} \]

in the fluidized bed region given by,

\[ \frac{dP}{dr} = (\rho_s - \rho_f)(1 - \varepsilon)r \omega^2 + \rho_f \varepsilon r \omega^2 + \frac{\rho_f U_o^2 r_o^2 \varepsilon}{\varepsilon^3 r^2} + \frac{\rho_f U_o^2 r_o^2}{\varepsilon^2 r^2} \frac{d\varepsilon}{dr} \]

however; in the fixed bed region the major contribution is from the drag force per unit volume, while in the fluidized bed region the major contribution is from the total mass of particles, therefore the above equations reduce to;

\[ \frac{dP}{dr} = \phi_1 \left( \frac{U_o r_o}{r} \right) + \phi_2 \left( \frac{U_o r_o}{r} \right)^2 \]

in the fixed bed region and to

\[ \frac{dP}{dr} = (\rho_s - \rho_f)(1 - \varepsilon)r \omega^2 \]

in the fluidized bed region. Integrating the above equations from \( r_1 \) to \( r_0 \) results in;

\[ \frac{U_{mf} \rho_f d_s}{\mu} = \left[ \left( \frac{33.7 C_2}{C_1} \right)^2 + 0.0408 \frac{\rho_f (\rho_s - \rho_f) d_s^2 \omega^2 C_3}{\mu^2 C_1} \right]^{-1/2} - 33.7 \frac{C_2}{C_1} \]
As we are not concerned with average fluidization velocity within the scope of this thesis, we will evaluate the above equation at \( r = r_o \) and introduce \( U_{mf} \) where the whole bed is fluidized, the result is;

\[
\frac{U_{mf} \rho_f d_g}{\mu} = \left[ (33.7)^2 + 0.0408 \frac{\rho_f (\rho_g - \rho_f) d_g \omega^2 r_o}{\mu^2} \right]^{1/2} - 33.7
\]

it is at this point that the partial fluidization graph joins the full fluidization graph, partial fluidization is given by;

\[
\Delta P = (1 - \varepsilon) \left( \rho_g - \rho_f \right) \omega^2 \left( r_{pf}^2 - r_i^2 \right) + \phi_1 U_o r_o \ln \left( \frac{r_o}{r_{pf}} \right) + \phi_2 U_o^2 r_o \left( \frac{1}{r_{pf}} - \frac{1}{r_o} \right)
\]

where \( r_{pf} \) is the interface of the fluidized and packed beds, full fluidization is given by;

\[
\Delta P_f = (1 - \varepsilon) \left( \rho_g - \rho_f \right) \omega^2 \left( r_o^2 - r_i^2 \right) / 2
\]

**NOTATION**

\( d_g \) = granule diameter

\( \Delta P \) = total pressure drop across fluidized bed

\( \Delta P_f \) = pressure drop across fluidized bed

\( r \) = radial coordinate

\( r_i \) = radius of inner surface of granule bed
\[ r_o = \text{radius of rotating fluidized bed} \]

\[ r_{pf} = \text{radius of interface between fluidized and packed bed} \]

\[ U_{mf} = \text{average minimum fluidization velocity} \]

\[ U_{mf_c} = \text{critical minimum fluidization velocity} \]

\[ U_o = \text{superficial air velocity based on outside radius} \]

\[ \varepsilon = \text{void fraction} \]

\[ \mu = \text{air viscosity} \]

\[ \rho_f = \text{air density} \]

\[ \rho_g = \text{granule density} \]

\[ \omega = \text{angular velocity} \]
APPENDIX D

INSTRUMENTATION OF RFB

A. U-Tube Manometer

In order that the pressure drop across the bed be measured differentially, a Dwyer™ U tube manometer 1 meter in length was installed with one lead in the plenum and the other in the exhaust.

B. Air Flow Rotometers

In order that the superficial air velocity be measured an array of three rotometers was purchased from Dwyer™ spanning air flow from 0 SCFH to 1800 SCFH.

WARNING: THE METERS SELECTED ARE RATED FOR 35 PSI MAX. PRESSURE, DURING A PROPERLY CONDUCTED EXPERIMENT THE PRESSURES DO NOT RISE ABOVE THIS RATING, IF THE EXHAUST IS CLOSED OFF OR THE AIR HOSES ARE CONNECTED IMPROPERLY, AN EXPLOSION OF THE METERS OR THE PLENUM MAY RESULT.

C. Motor Microcontroller

The Dayton™ DC motor is equipped with a microcontroller capable of 0 RPM to 1725 RPM in 1 RPM increments.

D. Miscellaneous Equipment

The compressed air was delivered by the native air compressor in the lab. 1/2 inch air lines from Coilhose® were required to deliver the desired rate of air flow. Exhaust was removed via 1 1/4 inch flexible tubing into the native fume hood
system in the lab. The nozzle runout was adjusted with the use of a Starret® dial indicator and stand.
REFERENCES


2. R. N. Dave, "Experiments and Simulations in Particle Technology" Notes from ME-717-102, NJIT, Spring 1998

3. I.S Fischer, "Introduction to Particle Technology", Notes from ME-717-001, NJIT, Fall 1997

4. K. Leschonski, "Short Course on Selected Topics of Particle Technology", Notes from Short Course, CUTC-Institute Ltd., Clausthal, Germany, 1998


